

In the Claims:

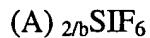
Please amend the claims as follows:

1. (Currently amended) A process for the catalytic dewaxing of a hydrocarbon oil feed obtained by the vacuum distillation of the residue of an atmospheric distillation of a crude petroleum feedstock, selected from the group consisting of solvent extracted waxy raffinate, gas oil and hydrocracker feedstock wherein said hydrocarbon oil feed includes waxy molecules and more than 1000 ppmw of sulphur or sulphur containing compounds and said hydrocarbon oil feed has not been subjected to a hydrotreating step to reduce sulfur and nitrogen content, by contacting the oil feed under catalytic dewaxing conditions with a catalyst composition comprising a Group VIII metal hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina.

Claim 2 (Canceled).

3. (Previously presented) The process of claim 1, in which the oil feed comprises more than 10 ppmw of nitrogen or nitrogen containing compounds.
4. (Previously presented) The process of claim 1, in which the hydrogenation component is platinum, palladium or nickel.
5. (Previously presented) The process of claim 1, in which the low acidity binder is silica.
6. (Previously presented) The process of claim 1, in which the aluminosilicate zeolite crystallites have a Constraint Index of between 2 and 12.
7. (Previously presented) The process of claim 6, in which the aluminosilicate zeolite crystallites include MFI type zeolite.

8. (Previously presented) The process of claim 1, in which the dealuminated aluminosilicate zeolite crystallites are obtained by contacting the zeolite crystallites with an aqueous solution of a fluorosilicate salt wherein the fluorosilicate salt is represented by the formula:



in which 'A' is a metallic or non-metallic cation other than H+ having the valence 'b'.

9. (Previously presented) The process of claim 8, in which an extrudate of the aluminosilicate zeolite crystallites and the low acidity binder is contacted with the aqueous solution of the fluorosilicate salt.

10. (Previously presented) The process of claim 1, in which the oil feed is a solvent extracted waxy raffinate.

11. (Previously presented) The process of claim 1, in which the oil feed is a gas oil.

12. (Previously presented) The process of claim 1, in which the oil feed is a hydrocracker feedstock and wherein the dewaxed oil is subsequently subjected to a hydrotreating step before being subjected to a hydrocracker process step in which step primarily middle distillates are prepared.

Claim 13 (canceled).

14. (Previously presented) The process of claim 8, where 'b' is ammonium.

15. (Previously presented) The process of claim 1, in which the hydrogenation component is palladium.

16. (Previously presented) The process of claim 1, in which the hydrogenation component is nickel.

17. (Currently amended) A process for the catalytic dewaxing of a hydrocarbon oil feed obtained by the vacuum distillation of the residue of an atmospheric distillation of a crude petroleum feedstock, selected from the group consisting of solvent extracted waxy raffinate, gas oil, and hydrocracker feedstock wherein said hydrocarbon oil feed includes waxy molecules and more than 1000 ppmw of sulphur or sulphur containing compounds and said hydrocarbon oil feed has not been subjected to a hydrotreating step to reduce sulfur and nitrogen content, by contacting said hydrocarbon oil feed under catalytic dewaxing conditions with a catalyst composition comprising a nickel hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina.

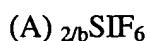
18. (Previously presented) The process of claim 17, wherein said hydrocarbon oil feed comprises more than 10 ppmw of nitrogen or nitrogen containing compounds.

19. (Previously presented) The process of claim 18, wherein said low acidity binder is silica.

20. (Previously presented) The process of claim 19, wherein said aluminosilicate zeolite crystallites have a Constraint Index of between 2 and 12.

21. (Previously presented) The process of claim 20, wherein said aluminosilicate zeolite crystallites include MFI type zeolite.

22. (Previously presented) The process of claim 21, wherein said dealuminated aluminosilicate zeolite crystallites are obtained by contacting the zeolite crystallites with an aqueous solution of a fluorosilicate salt wherein the fluorosilicate salt is represented by the formula:



in which 'A' is a metallic or non-metallic cation other than H+ having the valence 'b'.

23. (Previously presented) The process of claim 22, wherein an extrudate of the aluminosilicate zeolite crystallites and the low acidity binder is contacted with the aqueous solution of the fluorosilicate salt.

24. (Previously presented) The process of claim 23, wherein 'b' is ammonium.

25. (Previously presented) The process of claim 24, wherein said catalyst composition has an absence of a Group VIB metal component.

26. (Previously presented) The process of claim 9, wherein said catalyst composition has an absence of a Group VIB metal component.